

**ABS** INDUSTRIAL  
VERIFICATION (INDIA) PVT. LIMITED

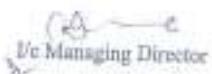
## 2. Financial / Commercial Details

The Financial / commercial data provided by the unit has not been certified by any certifying agency / Chartered accountant. But they agreed to provide the certified / audited financial data from next crushing season onwards. The data provided is self certified.

### 2.1 Financial Details as per annexure III of MEDA Tender document.

Calculation on the basis of 2011-12 Data.

Sr.No.	Financial / Commercial Data	Amount (Rs.)
1	Co-gen Project Cost Rs.	1496.08
2	Modernization Project Cost Rs.	--
3	Total Project Rs.	1496.08
4	Capital cost per MW with modernization	299.22
5	Capital cost per MW without modernization	299.22
6	Production cost Rs. / Unit	4.28
7	Cost of steam for Distillery Use Rs./MT Total cost Rs. Cr.	153.45
8	Cost of Electricity for Distillery Use Rs./Unit Total cost Rs. Cr.	31.62
9	Tariff considered Rs./Units	2.95
10	Total revenue / Cash accrual (Rs.Cr.) 2010-11	230.23
	2011-12	205.82
11	Debit Equity	NA
12	Equity 5 % SSK	NA
13	Equity 5 % State Govt.    It is applicable for New Projects only.	NA
14	SDF ( 36.46 %)	NA
15	FI/Bank (53.54 %)	NA
16	IRR (%)	NA
17	DSCR (Average )	NA
18	Break Even (%)	NA
19	Pay back period	NA

  
D/c Managing Director

Detailed Financial data is attached in annexure.

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1.5 Technical details as per annexure-III of MEDA Tender document:

Sr. No	TECHNICAL DATA	SEASON	OFF SEASON
1	Crushing Capacity Licensed	3500 TCD	-
2	Crushing Capacity Actual	3500 TCD	-
3	Crushing Capacity considered for Cogen Project (Average of last 5 years)	3860 TCD	-
4	Boiler Parameters- Pressure after Temp (oC/TPH) (Existing)	2.2 ATA   360 92.1 TPH	2.1 ATA 9.0 TPH
5	Boiler Parameters- Pressure after Temp (oC/TPH) (Existing)	2.1 ATA   365°C 9.0 TPH	1.9 Atm
6	T.G. Set Type & capacity (Existing)	Back press. 3.5 MW, 4795 kgs	-
7	T.G. Set Type & capacity (Existing)	2155 KVA	3.7 Mw
8	Operating days	106 days	-
9	Steam requirement TPH (Existing)	8.5 TPH	-
10	Steam consumption % on case for sugar (Existing)	4.0 %	-
11	Steam to HP Header TPH	-	-
12	Steam requirement to Distillery TPH (Existing)	6 TPH	-
13	Steam Required to deaerator TPH (Existing)	2.5 TPH	-
14	Steam through condenser TPH	-	-
15	Topping cycle efficiency % (>45%)	-	-
16	Thermal use % (>20%)	-	-
		-	-

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A.	FUEL UTILIZED	SEASON	OFF SEASON
1	Ratio of bagasse to steam (Existing)	1.1 - 2.2	-
2	Bagasse production % cane & TPH Biogas Equivalent Bagasse cane trash Total Bagasse Production MT	2.8 - 3.5 %	-
3	Bagasse used during season % cane/TPH Total Bagasse production MT	1.4 - 4.4 %	-
4	Bagasse saved % cane & MT	≤ 9.1 %	-
5	Bagasse used during off season TPH / Total Qty MT	6137 M.T.	-
6	Alternate Fuel used during season TPH/Total Qty MT Biogas- 1)	-	-

B.	POWER BALANCE	SEASON	OFF SEASON
1	Specific Steam Consumption / kWh/Beta/2 Sata	19 Kg / KWh	-
2	Power Generation MW / MUS	148994.24%	-
3	Captive Power MW /MUS	148913.50%	-
4	Power Export MW / MUS	78.796	-